

Important Formulas

Hydrostatic force on inclined plane surface	$F_h = \rho g h A$
Position of hydrostatic force on plane ($y_c = 0$)	$y_c = \bar{y} + \frac{I_{xc}}{y_c A}$
Position of hydrostatic force on plane ($y_c \neq 0$)	$y_c = \bar{y} + \frac{I_{xc}}{y_c A}$
Pressure variation in stationary (incompressible) fluid	$P_2 - P_1 = \rho g h$
Capillary rise in a tube ($\Delta h_{cap} = P_c, \Delta h_{cap} = 2\sigma \cos \theta$)	$h = \frac{2\sigma \cos \theta}{\rho g r}$
Buoyant force (by submerged or displaced volume)	$F_b = \rho V$
Metacenter loc	$\bar{M} = \bar{y} \bar{I}^2$
Metacenter for atmospheric pressure	$\bar{m} = \bar{y} + \frac{I_{xc}}{y_c A}$ $\bar{m} = \bar{y} + \frac{I_{xc}}{y_c A}$
Continuity of Flow	$Q = A_1 V_1 = A_2 V_2$
Velocity relationship in confined pipe	$V_1 = \frac{Q}{A_1} = \frac{Q}{\frac{\pi D_1^2}{4}}$ $V_2 = \frac{Q}{A_2} = \frac{Q}{\frac{\pi D_2^2}{4}}$
Velocity of flow through opening in large tank	$V = \sqrt{2gh}$
Vertical water velocity	$V_y = \frac{2V_m \left(1 - \frac{y^2}{R^2}\right)}{1 - \left(\frac{y^2}{R^2}\right)}$
Flow through a thin gate	$Q = C_{d1} b \sqrt{2gh} + C_{d2} \sqrt{2gh}^3$
Flow Through Broad Crest Weir	$Q = C_{d1} \sqrt{2g} H^{3/2}$
Flow through a sharp crested weir	$Q = C_{d1} \sqrt{2g} H^{3/2}$
Energy loss	$E = \frac{V^2}{2g} + z + \frac{V^2}{2g}$
Hydraulic grade line	$HGL = z + \frac{V^2}{2g} = \frac{P}{\rho g} + z$

Fluid Properties Relationship Tree



Fluid Dynamics

Velocity field	$\vec{V} = u\hat{i} + v\hat{j} + w\hat{k}$		
Acceleration field	$a_x = \frac{du}{dt} = \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z}$		
Accel of steady flow in streamline	$a = V \frac{dV}{ds} = \frac{V^2}{R}$		
	Change in V due to change in	Equal for every stream flow in	
Local Acceleration	$\frac{\partial V}{\partial t}$	Time	Steady
Convective Acceleration	$u \frac{\partial V}{\partial x} + v \frac{\partial V}{\partial y} + w \frac{\partial V}{\partial z}$	Position	Unsteady
Rayleigh Transport Theorem	$\frac{D}{Dt} \int_{CV} \rho \phi dV = \int_{CV} \rho \frac{D\phi}{Dt} dV + \int_{CS} \rho \phi (\vec{V} \cdot \vec{n}) dA$		

Bernoulli Equation

Valid for steady, incompressible, and inviscid flow. Only valid along a streamline. Only valid within a single continuous fluid.

Pressure form	$P_1 + \rho g y_1 + \frac{\rho V_1^2}{2} = P_2 + \rho g y_2 + \frac{\rho V_2^2}{2}$		
Energy head form	$\frac{P}{\rho g} + y + \frac{V^2}{2g} = \text{constant}$		
	$P = 0$	$V = 0$	$Z = 0$
At atmospheric surface	✓		
In free jet	✓		
At datum elevation			✓
At stagnation point		✓	
In large tank			✓
At top of free jet	✓	✓	
Impinging jets	ρ_{stagn}		

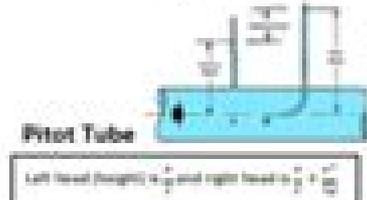
Streamline Function

$$\frac{dy}{dx} = \frac{v}{u} \Rightarrow u dy - v dx = 0 \Rightarrow \psi = \text{const}$$



Common Physical Properties / Units

	SI	Imperial
Atmospheric Pressure, P_{atm}	101.3 kPa	14.7 psi = 2116.3 lb/ft ²
Density ρ (H ₂ O)	1000 kg/m ³	1.940 slug/ft ³
Specific Weight γ (H ₂ O)	9810 N/m ³	62.4 lb/ft ³
Acid Gravity ρ	1.84 slug/ft ³	59.8 lb/ft ³
Length L	1 m = $\frac{1}{3.281}$ ft	1 ft = 0.3048 m
Mass, M	1 kg = 2.205 lbs 1 kg = 0.001102 slug	1 lbm = $\frac{1}{32.17}$ slug 1 slug = 32.17 lbm
Force, F	1 N = $\frac{1}{2.2}$ lbf	1 lbf = 4.45 N
Temperature, θ	1°C = 1.8°F	1°F = $\frac{1}{1.8}$ °C
Volume, V	1 m ³ = 35.31 ft ³	1 ft ³ = 0.0283 m ³



Properties of 2-D Shapes

	$A = bh$ $I_x = \frac{1}{12}bh^3$ $I_y = \frac{1}{12}b^3h$ $I_{xc} = 0$
	$A = \pi R^2$ $I_x = I_y = \frac{\pi R^4}{4}$ $I_{xc} = 0$
	$A = \frac{\pi R^2}{2}$ $I_x = \frac{\pi R^4}{8}$ $I_y = \frac{\pi R^4}{16}$ $I_{xc} = 0$
	$A = \frac{1}{2}bh$ $I_x = \frac{bh^3}{36}$ $I_y = \frac{b^3h}{36}$ $I_{xc} = \frac{bh^3}{36} - bh^2$
	$A = \frac{\pi R^2}{4}$ $I_x = I_y = 0.1098R^4$ $I_{xc} = -0.0549R^4$

Fluids Exam Answer Sheet

Patricia A. Hoefler



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